42-045-00070
B Augustine

Monroe Energy, LLC
4101 Post Road
Trainer, PA 19061
(610) 364-8000

January 28, 2019

FEDEX: 774311692611

Mr. James Rebarchak
Commonwealth of Pennsylvania
Department of Environmental Protection
Southeast Regional Office
2 East Main Street
Norristown, PA 19401

Re: Monroe Energy, LLC – Trainer Refinery
40 CFR 63, Subpart UUU Semiannual Report
Reporting Period: July 1, 2018 – December 31, 2018

Mr. Rebarchak:

In accordance with 40 CFR 63 Subpart UUU, Monroe Energy, LLC's Trainer Refinery hereby submits this semi-annual compliance report (per §63.1575(b)(2)) for the period beginning July 1, 2018 and ending December 31, 2018. Compliance reporting for the applicable MACT II emission limitations and work practices are detailed in the enclosed appendices.

Should you have any questions or comments regarding this report, please contact me at (610) 742-6633, or, at (610) 364-8399.

Matthew Torell, P.E.

Environmental Leader

Enclosure

cc: Office of Air Enforcement and Compliance Assistance (3AP20)
U.S. EPA, Region III
1650 Arch Street
Philadelphia, Pa 19103-2029
FEDEX: 774311711323

Bcc: \\TRN-FS01\shared\HSE\!ENVIRONMENTAL\10 AIR\03 REPORTS\3.2 Semi-Annual MACT UUU & NSPS J Report\Reporting Year 2018\2H2018

Monroe Energy, LLC
4101 Post Road
Trainer, PA 19061
(610) 364-8000

Responsible Official Certification

Based upon information and belief formed after a reasonable inquiry, I, as a responsible official of the above-mentioned facility, certify the information contained in this report is accurate and true to the best of my knowledge.

1/28/2019

Michael Capone,
Refinery Leader

Appendix A-Excess Emission and Monitoring System Performance Summary

EXCESS EMISSION AND MONITORING SYSTEM PERFORMANCE SUMMARY REPORT

Pollutant (Circle One): SO_2 NO_X TRS H_2S (CO) Opacity

Reporting period dates: From **July 1, 2018** to **December 31, 2018**

Company: **Monroe Energy, LLC**

Emission Limitation: **500 ppm (1-hour average)**

Address: **4101 Post Rd, Trainer PA 19061**

Monitor Manufacturer: **Servomex**

Model No.: **04900C1-4202**

Date of Latest CMS Certification or Audit: **12/27/2018 (Linearity Test)**

Process Unit(s) Description: **FCCU**

Total source operating time in reporting period : **3091 hours**

Emission data summary [1]		CMS performance summary [1]	
1. Duration of excess emissions in the reporting period due to:		1. CMS downtime in the reporting period due to:	
a. Startup/shutdown	1	a. Monitor equipment malfunctions	0
b. Control equipment problems	0	b. Non-Monitor equipment malfunctions	0
c. Process problems	0	c. Quality assurance calibration	0
d. Other known causes	0	d. Other known causes	0
e. Unknown causes	0	e. Unknown causes	77
2. Total duration of excess emissions	1	2. Total CMS Downtime	77
3. Total duration of excess emissions x (100) / [Total source operating time]	0.03 %	3. [Total CMS Downtime] x (100) / [Total source operating time]	2.50 %

Notes:

On a separate page, describe any changes since last quarter in CMS, process or controls. **No changes to the CMS, process, or controls have occurred since last reporting period.**

EXCESS EMISSION AND MONITORING SYSTEM PERFORMANCE SUMMARY REPORT

Pollutant (Circle One): (SO_2) NO_x TRS H_2S CO Opacity

Reporting period dates: From **July 1, 2018** to **December 31, 2018**

Company: **Monroe Energy, LLC**

Emission Limitation: **250 ppm (12- hour rolling average)**

Address: **4101 Post Rd, Trainer PA 19061**

Monitor Manufacturer: **AMETEK**

Model No.: **Model 921**

Date of Latest CMS Certification or Audit: **12/18/2018 (Linearity Test)**

Process Unit(s) Description: **Claus Sulfur Recovery Plant**

Total source operating time in reporting period: **3855 hours**

Emission data summary [1]		CMS performance summary [1]	
1. Duration of excess emissions in the reporting period due to:		1. CMS downtime in the reporting period due to:	
a. Startup/shutdown	0	a. Monitor equipment malfunctions	0
b. Control equipment problems	0	b. Non-Monitor equipment malfunctions	0
c. Process problems	28	c. Quality assurance calibration	0
d. Other known causes	0	d. Other known causes	0
e. Unknown causes	0	e. Unknown causes	52
2. Total duration of excess emissions	28	2. Total CMS Downtime	52
3. Total duration of excess emissions x (100) / [Total source operating time]	0.73 %	3. [Total CMS Downtime] x (100) / [Total source operating time]	1.30 %

*There is a process analyzer on the SRU stack, which is not a CEMS, but is used for other process control purposes. This analyzer suggests that there were a total of 7 hours of excess emissions. However, we are reporting the actual CEMS based excess emissions for consistency with the regulation.

Note: On a separate page, describe any changes since last quarter in CMS, process or controls. **No changes to the CMS, process, or controls have occurred since last reporting period.**

Appendix B-UUU Deviation Summary and Corrective Actions

If any deviations occur from standards that use CEMS for compliance, refer to Appendix E to view detailed CEMS downtime information.

Source: SRU
Standard: 250 PPM SO2 12-Hr Rolling Average Limit

Start	Stop	Duration	Caused by SSM event?	Nature and Cause of Event?	Corrective Action Taken?
8/12/2018 19:00	8/13/2018 1:59	7 hours	No	Upset conditions at sour water and amine units caused an emission exceedance at the SRU.	Erratic gas flow was stabilized and unit returned to normal operations.
11/18/2018 23:00	11/19/2018 2:59	4 hours	Yes	Startup related process issues caused a steam upset at the sour water and amine units, affecting SRU operations.	Steam issue was stabilized and erratic flows of acid gas and sour water stabilized returning the unit to normal operations.
12/15/2018 18:00	12/16/2018 10:59	17 hours	No	Upset conditions at sour water and amine units caused an emission exceedance at the SRU.	Sour Water and Amine operating conditions were returned to normal and the SRU returned to normal operating conditions.

Source: FCCU
Standard: 500 PPMVD CO 1-Hr Average Limit

Start	Stop	Duration	Caused by SSM event?	Nature and Cause of Event?	Corrective Action Taken?
9/28/2018 0:00	9/28/2018 0:59	1 hour	Yes	Shutdown of the FCC caused process upset conditions that resulted in an emissions exceedance.	FCC Unit was shutdown.

Source: FCCU
Standard: L:G Ratio ≥ 0.08 (Per November 22, 2005 AMP) – Demonstrates §63.1564 Compliance for PM and Opacity Standards

There were no deviations from this standard during the reporting period.

Source:	Platformer
Standard:	%97% HCl reduction with a control device; weekly average Chloride content on catalyst entering Chlorsorb ≤ 1.35% by weight and weekly average Chloride content on catalyst exiting Chlorsorb ≤ 1.8% by weight, 3 times per week on non-consecutive days during catalyst regeneration.

There were no deviations from this standard during the reporting period.

Source:	Platformer
Standard:	Daily Average Vet Gas Inlet Temperature ≤ 350°F

There were no deviations from this standard during the reporting period.

Appendix C-Process Descriptions

FCCU Process Description

The Fluidized Catalytic Cracking Unit (FCCU) is a refinery process unit used for the production of gasoline. Heavy oil, which is used as the feedstock, is catalytically cracked in a fluidized catalyst bed to produce C3 olefins, C4 olefins, and isobutanes. In the cracking reactor, heavy carbonaceous materials (coke) become deposited on the catalyst, requiring continuous regeneration. The catalyst is circulated to a fluidized bed regenerator where these deposits are combusted. Most of the catalyst particles entrained in the regenerator flue gas are then removed in two stages of cyclones within the regenerator vessel and then are returned to the fluidized bed reactor.

At the Trainer Refinery, the FCCU control devices include a CO Boiler for CO reduction, an Enhanced Selective Non-Catalytic Reduction (eSNCR) unit for NO_x reduction, an electrostatic precipitator for PM reduction and a wet gas scrubber for PM and SO_2

Catalytic Reforming Unit (Platformer Unit)

The refinery operates one Catalytic Reforming Unit. The purpose of the Platformer is to upgrade low octane feed sources, Heavy Naphtha and Heavy Isocrackate, into a high-octane gasoline component and hydrogen gas. The feed combined with hydrogen recycle gas is heated and passed over a platinum catalyst, where it is converted from low octane naphtha to a gasoline-blending component with a design research octane number in the range of 97 - 101.

SRU

The Claus Sulfur Recovery Unit is designed to react feed H_2S and SO_2 into recoverable sulfur using two trains in parallel. Normally only one train is required to be on-line. The feeds to the unit are sour water gases and acid gases from the Sour Water Stripper and the Amine Unit. Each train consists of a thermal reactor, three catalytic reactors, a steam generator and a 4 pass sulfur condenser. Medium and low-pressure steam is generated in the condensers. The sulfur product is stored in a common heated pit until shipped out by railcar.

The Scot unit is designed to treat the tail gas from both trains of the Sulfur Recovery Unit. The Scot Unit reduces the H_2S content in the tail gas before it is sent to the incinerator stack. The combination of the Sulfur and Scot Units recovers about 99.8% of the sulfur in the feed streams. The Scot Unit consists of an in-line burners, catalytic reactor, quench tower, amine absorber, stripper, and incinerator.

Bypass Lines

The FCCU does not have any bypass lines. The Platformer Chlorsorb Unit line was not bypassed during this reporting period. The Sulfur Recovery Unit line was not bypassed during this reporting period.

Appendix D-Performance Testing Information

Monroe Energy, LLC conducted 2 Particulate Matter (PM) performance tests during the reporting period. The summary of the test results are included in this report.

Table 5-1
Monroe Energy, LLC - Trainer, PA
FCCU Scrubber Stack
Summary of Particulate Test Data and Test Results

TEST DATA:				
Test run number	1	2	3	
Loaction		FCCU Scrubber Stack		
Test date	09/12/18	09/12/18	09/12/18	
Test time period	0915-1053	1228-1403	1443-1617	
Coke burn rate, 1000 lbs/hr	33.461	33.218	33.102	
SAMPLING DATA:				
Sampling duration, min.	84	84	84	
Nozzle diameter, in.	0.290	0.300	0.302	
Cross sectional nozzle area, sq.ft.	0.000459	0.000491	0.000497	
Barometric pressure, in. Hg	30.20	30.22	30.22	
Avg. orifice press. diff., in H_2O	1.53	1.70	1.85	
Avg. dry gas meter temp., deg F	69.5	68.9	70.6	
Avg. abs. dry gas meter temp., deg. R	530	529	531	
Total liquid collected by train, ml	347.4	387.3	404.5	
Std. vol. of H_2O vapor coll., cu.ft.	16.4	18.2	19.0	
Dry gas meter calibration factor	0.9916	0.9916	0.9916	
Sample vol. at meter cond., dcf	52.579	54.536	58.097	
Sample vol. at std. cond., dscf [1]	52.650	54.729	58.141	
Percent of isokinetic sampling	99.1	98.7	100.7	
GAS STREAM COMPOSITION DATA:				
CO_2, % by volume, dry basis	15.3	15.0	15.1	
O_2, % by volume, dry basis	2.5	2.6	2.4	
N_2, % by volume, dry basis	82.2	82.4	82.5	
Molecular wt. of dry gas, lb/lb mole	30.55	30.50	30.51	
H_20 vapor measured in gas stream, prop. by vol.	0.237	0.250	0.247	
H_2O vapor in gas stream, (saturated quantity)[2][3]	0.245	0.245	0.248	
Mole fraction of dry gas	0.763	0.755	0.753	
Molecular wt. of wet gas, lb/lb mole	27.57	27.44	27.42	
GAS STREAM VELOCITY AND VOLUMETRIC FLOW DATA:				
Static pressure, in. H_2O	-0.28	-0.28	-0.25	
Absolute pressure, in. Hg	30.18	30.20	30.20	
Avg. temperature, deg. F	149.1	149.2	149.6	
Avg. absolute temperature, deg.R	609	609	610	
Pitot tube coefficient	0.84	0.84	0.84	
Total number of traverse points	12	12	12	
Avg. gas stream velocity, ft./sec.	34.5	34.0	35.01	
Stack/duct cross sectional area, sq.ft.	103.87	103.87	103.87	
Avg. gas stream volumetric flow, wacf/min.	214728	211740	218189	
Avg. gas stream volumetric flow, dscf/min.	143192	139711	143590	
PARTICULATE LABORATORY REPORT DATA				
Front half acetone rinse, g	0.1191	0.0549	0.1011	
Filter, g	0.0455	0.0553	0.0583	
Filterable particulate catch weight, g	0.1646	0.1102	0.1594	
FILTERABLE PARTICULATE EMISSIONS (EPA M5B)				Average
Conc., gr/dscf	0.0482	0.0311	0.0423	0.0405
Emission rate, lbs/hr	59.21	37.21	52.07	49.50
Emission rate, lb/1000 lb coke burned	1.770	1.120	1.573	1.488

(1) Standard conditions = 68 deg. F. (20 deg. C.) and 29.92 inches Hg (760mm Hg).

(2) H_2O vapor saturated quantity is based on stack gas temperature and psychrometry.

(3) The lower of the saturated or measured moisture was selected to calculate the volumetric flow rate.

MONROE ENERGY LLC, TRAINER, PA
FCCU SCRUBBER STACK
SUMMARY OF PARTICULATE TEST DATA AND TEST RESULTS

TEST DATA:				
Test run number	1	2	3	
Loaction		FCCU Scrubber Stack		
Test date	12/20/18	12/20/18	12/20/18	
Test time period	0846-1022	1059-1235	1340-1515	
Coke burn rate, 1000 lbs/hr	38.75	38.81	39.49	
SAMPLING DATA:				
Sampling duration, min.	84	84	84	
Nozzle diameter, in.	0.281	0.274	0.275	
Cross sectional nozzle area, sq.ft.	0.000431	0.000409	0.000412	
Barometric pressure, in. Hg	30.09	30.08	30.00	
Avg. orifice press. diff., in H_2O	1.55	1.47	1.42	
Avg. dry gas meter temp., deg F	72.1	72.8	72.8	
Avg. abs. dry gas meter temp., deg. R	532	533	533	
Total liquid collected by train, ml	308.0	306.6	343.6	
Std. vol. of H_2O vapor coll., cu.ft.	14.5	14.4	16.2	
Dry gas meter calibration factor	0.9890	0.9890	0.9890	
Sample vol. at meter cond., dcf	55.781	54.975	54.442	
Sample vol. at std. cond., dscf [1]	55.237	54.347	53.666	
Percent of isokinetic sampling	95.7	98.5	99.5	
GAS STREAM COMPOSITION DATA:				
CO_2, % by volume, dry basis	14.8	15.0	15.1	
O_2, % by volume, dry basis	2.8	2.8	2.5	
N_2, % by volume, dry basis	82.4	82.2	82.4	
Molecular wt. of dry gas, lb/lb mole	30.48	30.51	30.52	
H_20 vapor measured in gas stream, prop. by vol.	0.208	0.210	0.232	
H_2O vapor in gas stream, (saturated quantity)[2][3]	0.213	0.219	0.223	
Mole fraction of dry gas	0.792	0.790	0.777	
Molecular wt. of wet gas, lb/lb mole	27.89	27.89	27.72	
GAS STREAM VELOCITY AND VOLUMETRIC FLOW DATA:				
Static pressure, in. H_2O	-0.30	-0.32	-0.35	
Absolute pressure, in. Hg	30.07	30.06	29.97	
Avg. temperature, deg. F	143.3	144.4	145.2	
Avg. absolute temperature, deg.R	603	604	605	
Pitot tube coefficient	0.84	0.84	0.84	
Total number of traverse points	12	12	12	
Avg. gas stream velocity, ft./sec.	38.20	38.60	38.23	
Stack/duct cross sectional area, sq.ft.	103.87	103.87	103.87	
Avg. gas stream volumetric flow, wacf/min.	238051	240540	238257	
Avg. gas stream volumetric flow, dscf/min.	165763	166725	161748	
PARTICULATE LABORATORY REPORT DATA				
Front half acetone rinse, g	0.0187	0.0082	0.0027	
Filter, g	0.0073	0.0181	0.0352	
Filterable particulate catch weight, g	0.0260	0.0263	0.0379	
FILTERABLE PARTICULATE EMISSIONS (EPA M5B)				
Conc., gr/dscf	0.0073	0.0075	0.0109	**Average**
Emission rate, lbs/hr	10.32	10.67	15.11	**12.03**
Emission rate, lb/1000 lb coke burned	0.266	0.275	0.383	**0.308**

"<" = Detection limit value, not included in emission rate calculations

(1) Standard conditions = 68 deg. F. (20 deg. C.) and 29.92 inches Hg (760mm Hg).

(2) H_2O vapor saturated quantity is based on stack gas temperature and psychrometry.

Appendix E - Detailed CEMS Downtime

Both the FCC and the SRU had limit exceedances in the second half of 2018. Therefore, the detailed CEMS downtime report is included below.

Downtime Events - Duration

Plant: MONROE ENERGY, LLC.
Report Period: 07/01/2018 00:00 Through 12/31/2018 23:59
Time Online Criteria: 1 minute(s)

Source: FCCSTACK
Parameter: CO
Interval: 001H

Incident ID	Start Date/Time	End Date/Time	Duration (hh:mm)	Reason Code - Description Action Code - Description
1	07/01/2018 05:00	07/01/2018 05:59	1h - 0m	00 - None
				00 - None
2	07/02/2018 05:00	07/02/2018 05:59	1h - 0m	00 - None
				00 - None
3	07/03/2018 05:00	07/03/2018 05:59	1h - 0m	00 - None
				00 - None
4	07/04/2018 05:00	07/04/2018 05:59	1h - 0m	00 - None
				00 - None
5	07/05/2018 05:00	07/05/2018 05:59	1h - 0m	00 - None
				00 - None
6	07/09/2018 07:00	07/09/2018 07:59	1h - 0m	00 - None
				00 - None
7	07/17/2018 08:00	07/17/2018 08:59	1h - 0m	00 - None
				00 - None
8	07/21/2018 05:00	07/21/2018 09:59	5h - 0m	00 - None
				00 - None
9	07/22/2018 05:00	07/22/2018 09:59	5h - 0m	00 - None
				00 - None
10	07/23/2018 05:00	07/23/2018 09:59	5h - 0m	00 - None
				00 - None
11	07/27/2018 08:00	07/27/2018 08:59	1h - 0m	00 - None
				00 - None
12	08/02/2018 08:00	08/02/2018 08:59	1h - 0m	00 - None
				00 - None
13	08/16/2018 07:00	08/16/2018 07:59	1h - 0m	00 - None
				00 - None
14	08/17/2018 10:00	08/17/2018 10:59	1h - 0m	00 - None
				00 - None
15	08/18/2018 07:00	08/18/2018 07:59	1h - 0m	00 - None
				00 - None
16	08/19/2018 00:00	08/19/2018 16:59	17h - 0m	00 - None
				00 - None
17	08/21/2018 07:00	08/21/2018 07:59	1h - 0m	00 - None
				00 - None
18	08/22/2018 01:00	08/22/2018 08:59	8h - 0m	00 - None
				00 - None
19	08/24/2018 08:00	08/24/2018 08:59	1h - 0m	00 - None
				00 - None
20	08/28/2018 07:00	08/28/2018 07:59	1h - 0m	00 - None
				00 - None

* Indicates duration incident could have additional data prior to the start date or following the end date.

Downtime Events - Duration

Plant: MONROE ENERGY, LLC.
Report Period: 07/01/2018 00:00 Through 12/31/2018 23:59
Time Online Criteria: 1 minute(s)

Source: FCCSTACK
Parameter: CO
Interval: 001H

Incident ID	Start Date/Time	End Date/Time	Duration (hh:mm)	Reason Code - Description Action Code - Description
21	09/03/2018 09:00	09/03/2018 09:59	1h - 0m	00 - None
				00 - None
22	09/04/2018 11:00	09/04/2018 11:59	1h - 0m	00 - None
				00 - None
23	09/05/2018 10:00	09/05/2018 10:59	1h - 0m	00 - None
				00 - None
24	09/09/2018 09:00	09/09/2018 09:59	1h - 0m	00 - None
				00 - None
25	09/13/2018 07:00	09/13/2018 07:59	1h - 0m	00 - None
				00 - None
26	09/17/2018 08:00	09/17/2018 08:59	1h - 0m	00 - None
				00 - None
27	09/26/2018 07:00	09/26/2018 12:59	6h - 0m	00 - None
				00 - None
28	09/26/2018 14:00	09/26/2018 14:59	1h - 0m	00 - None
				00 - None
29	09/27/2018 07:00	09/27/2018 13:59	7h - 0m	00 - None
				00 - None
30	11/19/2018 15:00	11/19/2018 15:59	1h - 0m	00 - None
				00 - None
31	12/27/2018 09:00	12/27/2018 09:59	1h - 0m	00 - None
				00 - None
		Number of Events:	31	
		Total Duration:	77h - 0m	

* Indicates duration incident could have additional data prior to the start date or following the end date.

Downtime Events - Duration

Plant: MONROE ENERGY, LLC.
Report Period: 07/01/2018 00:00 Through 12/31/2018 23:59
Time Online Criteria: 1 minute(s)

Source: SRUSTACK
Parameter: O2
Interval: 001H

Incident ID	Start Date/Time	End Date/Time	Duration (hh:mm)	Reason Code - Description Action Code - Description
1	07/16/2018 09:00	07/16/2018 09:59	1h - 0m	00 - None
				00 - None
2	08/22/2018 07:00	08/22/2018 07:59	1h - 0m	00 - None
				00 - None
3	08/22/2018 09:00	08/22/2018 10:59	2h - 0m	00 - None
				00 - None
4	08/22/2018 12:00	08/22/2018 13:59	2h - 0m	00 - None
				00 - None
5	08/29/2018 07:00	08/29/2018 07:59	1h - 0m	00 - None
				00 - None
6	11/06/2018 16:00	11/06/2018 16:59	1h - 0m	00 - None
				00 - None
7	11/07/2018 05:00	11/07/2018 08:59	4h - 0m	00 - None
				00 - None
8	11/08/2018 05:00	11/08/2018 08:59	4h - 0m	00 - None
				00 - None
9	11/09/2018 09:00	11/09/2018 09:59	1h - 0m	00 - None
				00 - None
10	11/12/2018 05:00	11/12/2018 07:59	3h - 0m	00 - None
				00 - None
11	11/18/2018 05:00	11/18/2018 09:59	5h - 0m	00 - None
				00 - None
12	11/29/2018 17:00	11/30/2018 07:59	15h - 0m	00 - None
				00 - None
13	12/07/2018 06:00	12/07/2018 06:59	1h - 0m	00 - None
				00 - None
		Number of Events:	13	
		Total Duration:	41h - 0m	

Source: SRUSTACK
Parameter: SO2
Interval: 001H

Incident ID	Start Date/Time	End Date/Time	Duration (hh:mm)	Reason Code - Description Action Code - Description
14	07/02/2018 09:00	07/02/2018 10:59	2h - 0m	00 - None
				00 - None
15	07/08/2018 05:00	07/08/2018 08:59	4h - 0m	00 - None
				00 - None
16	07/14/2018 05:00	07/14/2018 06:59	2h - 0m	00 - None
				00 - None

* Indicates duration incident could have additional data prior to the start date or following the end date.

Downtime Events - Duration

Plant: MONROE ENERGY, LLC.
Report Period: 07/01/2018 00:00 Through 12/31/2018 23:59
Time Online Criteria: 1 minute(s)

Source: SRUSTACK
Parameter: SO2
Interval: 001H

Incident ID	Start Date/Time	End Date/Time	Duration (hh:mm)	Reason Code - Description Action Code - Description
17	07/23/2018 10:00	07/23/2018 10:59	1h - 0m	00 - None
				00 - None
18	08/22/2018 07:00	08/22/2018 07:59	1h - 0m	00 - None
				00 - None
19	08/22/2018 09:00	08/22/2018 10:59	2h - 0m	00 - None
				00 - None
20	08/22/2018 12:00	08/22/2018 13:59	2h - 0m	00 - None
				00 - None
21	11/07/2018 05:00	11/07/2018 08:59	4h - 0m	00 - None
				00 - None
22	11/09/2018 09:00	11/09/2018 09:59	1h - 0m	00 - None
				00 - None
23	11/13/2018 05:00	11/13/2018 08:59	4h - 0m	00 - None
				00 - None
24	11/14/2018 05:00	11/14/2018 09:59	5h - 0m	00 - None
				00 - None
25	11/29/2018 17:00	11/30/2018 07:59	15h - 0m	00 - None
				00 - None
26	12/01/2018 05:00	12/01/2018 08:59	4h - 0m	00 - None
				00 - None
27	12/03/2018 05:00	12/03/2018 08:59	4h - 0m	00 - None
				00 - None
28	12/06/2018 06:00	12/06/2018 06:59	1h - 0m	00 - None
				00 - None
29	12/07/2018 06:00	12/07/2018 06:59	1h - 0m	00 - None
				00 - None
30	12/27/2018 06:00	12/27/2018 07:59	2h - 0m	00 - None
				00 - None
		Number of Events:	17	
		Total Duration:	55h - 0m	

* Indicates duration incident could have additional data prior to the start date or following the end date.